Exergetic and Sustainability Evaluation of a Building Heating System in Izmir, Turkey

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Abstract—Heating, cooling and lighting appliances in buildings account for more than one third of the world's primary energy demand. Therefore, main components of the building heating systems play an essential role in terms of energy consumption. In this context, efficient energy and exergy utilization in HVAC-R systems has been very essential, especially in developing energy policies towards increasing efficiencies. The main objective of the present study is to assess the performance of a family house with a volume of 326.7 m³ and a net floor area of 121 m², located in the city of Izmir, Turkey in terms of energetic, exergetic and sustainability aspects. The indoor and exterior air temperatures are taken as 20°C and 1°C, respectively. In the analysis and assessment, various metrics (indices or indicators) such as exergetic efficiency, exergy flexibility ratio and sustainability index are utilized. Two heating options (Case 1: condensing boiler and Case 2: air heat pump) are considered for comparison purposes. The total heat loss rate of the family house is determined to be 3770.72 W. The overall energy efficiencies of the studied cases are calculated to be 49.4% for Case 1 and 54.7% for Case 2. The overall exergy efficiencies, the flexibility factor and the sustainability index of Cases 1 and 2 are computed to be around 3.3%, 0.17 and 1.034, respectively.

Keywords—Buildings, exergy, low exergy, sustainability, efficiency, heating, renewable energy.

I. INTRODUCTION

In many countries, reducing fossil energy utilization and promoting renewable energies in the building sector have been very essential due to global warming considerations. Reductions in energy utilization can be achieved by minimizing the energy demand, rational energy utilization, recovering heat and cold and using energy from the ambient air and the ground. For keeping the environmental impact of a building at sustainable levels (e.g., by greenhouse gas neutral emissions), the residual energy demand must be covered with renewable energy [1].

Buildings consume energy throughout their whole life cycles, and many aspects and stages of building development and utilization impact their energy and environmental performances, from planning, design, construction and installation to test, commissioning, operation and maintenance [2].

The concept of exergy and exergy-economics has been attracted more and more attentions. Exergy analysis, which is a way to sustainability and reflects the extent of energy utilization, veritably provides a new assessment method of energy efficiency [3]. Exergy may be defined in various ways [4] and indicates the maximum work potential of a system under certain conditions. All systems with different conditions from the environment contain exergy.

Exergy analysis method has been applied to various building heating systems using the low exergy (LowEx) approach in recent years to assess their performances from the primary energy production to the building envelope, as comprehensively reviewed by Hepbasli elsewhere [4].

The key issue is how to make buildings both energetically and exergetically sustainable. Exergy as a thermodynamic analysis tool may help achieve this objective. The LowEx approach is one of these approaches, which has been and still being successfully used in the design of sustainable buildings. In recent years, the number of various studies on LowEx heating/cooling systems, of which flow temperatures are very close to the room to be heated/cooled, has dramatically increased. Through the LowEx approach, the energy/exergy flows from the primary energy production to the building envelope are determined to indicate the potential for further improvements in the energy and exergy utilization at each stage of the building heating/cooling system.

Considering some LowEx studies, Balta et al. [5] investigated a ground source heat pump and a low exergy heating system. They presented energy and exergy flows for the selected building boundary conditions. Hasan et al. [6] assessed the performance of a building by using a dynamic simulation. Low temperature water heating system was compared with radiator and floor heating systems. Based on the results, the low temperature water heating system had more appropriate temperature levels. Yucer and Hepbasli [7] exergetically evaluated a building heating system serving for educational purposes. They investigated the system performance by stages, namely generation, distribution, emission, and building envelope while presenting energy and exergy flows of the building investigated.

The main objective of this contribution is to apply the Lowex approach to a family house from the generation stage to the building envelope to reveal the inefficiencies of the components and their interrelations.

II. SYSTEM DESCRIPTION

In this study, a family house with a volume of 326.7 m^3 and a net floor area of 121 m^2 is considered as a case study [8]. The winter design outside temperature is 0°C for the city of Izmir while the design outside temperature can be taken as 1°C with 99.6% frequency [9]. That means the heating system

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(Table II).

consist of brick for the walls, plaster for interior and exterior

surfaces, reinforced concrete floors, ceilings, XPS and glass

wool insulation. For this study, insulation, in accordance with

the current Turkish building standard [10], in walls and ceiling

as well as windows, the window shading was considered

will provide a thermal comfort at 99.6% of the time, but may fail to do so during 0.4% of the time. The indoor air temperature is taken as 20°C. The plan and panoramic view of the house is shown in Fig. 1. The architectural features, such as direction and size of walls and windows, are listed in Table I.

The construction materials are locally manufactured and



Fig. 1 Plan and panoramic view of the considered family house [8]

THE ARCHITECTURAL FEATURES OF THE HOUSE												
	Space Area	Dimention		Walls		Windows			Doors			Net Wall Area
Space	(m ²)	Direction	(m)	(m)	(m ²)	(m)	(m)	(m ²)	(m)	(m)	(m ²)	(m ²)
Saloon	20	G	5	2.7	13.5	1.5	1.3	1.95	2	2.2	4.4	7.15
Saloon	50	D	6	2.7	16.2	3	1.3	3.9				12.3
Doront Doom	175	D	3.5	2.7	9.45							9.45
Falent Koom	17.5	K	5	2.7	13.5	1.5	1.3	1.95				11.55
Parent Bathroom	6	D	1.5	2.7	4.05	0.6	0.6	0.36				3.69
Padroom 1	17.5	K	5	2.7	13.5	1.5	1.3	1.95				11.55
Bedroom-1		В	3.5	2.7	9.45	1.5	1.3	1.95				7.5
Dadraam 2	12.25	В	3.5	2.7	9.45	1,5	1.3	1.95				7.5
Bedroom-2	12.23	G	1.5	2.7	4.05							4.05
Vitahan	14	В	4	2.7	10.8	1.5	1.3	1.95				8.85
Kitchell	14	G	3.5	2.7	9.45				2	2.2	4.4	5.05
Bathroom	10	D	2	2.7	5.4	0.6	0.6	0.36				5.04
Hall	13.75	В	2	2.7	5.4				1	2.2	2.2	3.2
TOTAL	121				124.2			16.32			11	96.88

TABLE II

THE THICKNESS AND CALCULATED U (THERMAL TRANSMITTANCE) VALUES OF THE BUILDING CONSTRUCTION MATERIALS

Lavora	Thermal Conductivity	Exterior Wall	Ceiling	Floor
Layers	(W/mK)	(m)	(m)	(m)
Inner Plaster	1.4	0.015	0.015	0.02
Brick	0.68	0.19	-	-
Reinforced cement	-	-	0.15	0.20
Exterior Plaster	1.4	0.015	0.015	0.02
Sand-Gravel	2.0	-	-	0.10
XPS insulation	0.04	0.05	-	
Glass wool	0.04	-	0.08	0.05
U-(Thermal transmittance)	(W/m^2K)	0.581	0.447	0.615

Fig. 2 shows the energy flows in forms of primary and electricity for a building from the primary energy transformation through the heat generation system and the

distribution system to the heating system, and from there, via the indoor air, across the building envelope to the surrounding air.

For the heating applications, two options are studied with 1a condensing boiler and 2- an air heat pump. The radiators are considered as heating systems. The distribution systems are considered to have good insulation. The domestic hot water (DHW) energy demand is ignored in this study.

III. ANALYSIS

The energy and exergy analyses of the considered systems are made through an Excel tool, which has been developed within the framework of International Energy Agency (IEA) formed within the Energy Conservation in Buildings and Community Systems Programme (ECBCSP) Annex 37 [11]. The tool and the calculation approach follow the method developed by Schmidt [12]. The main equations of the energy and exergy analyses are listed in Tables III and IV.

MAIN EQUATIONS OF ENERGY ANALYSIS							
Heat Losses							
Transmission heat loss rate [W]	$Q_T = \sum (U_i . A_i . F_{xi}) (T_i - T_o)$	(1)					
Ventilation heat loss rate [W]	$\dot{Q}_V = \left(c_p \cdot \rho \cdot V \cdot n_d \cdot (1 - \eta_V)\right) \left(T_i - T_o\right)$	(2)					
Heat Gains							
Solar heat gain rate [W]	$\dot{Q}_{s} = \sum \left(I_{s,j} \cdot (1 - F_{f}) \cdot A_{w,j} \cdot g_{j} \cdot F_{sh} \cdot F_{no} \right)$	(3)					
Internal gain rate of occupants [W]	$\dot{Q}_{O} = \dot{Q}_{O}''.no_{O}$	(4)					
Internal gain rate of equipment [W]	$\dot{Q}_e = \dot{Q}_e''.A_N$	(5)					
Other Uses							
Lighting power [W]	$P_l = p_l . A_N = \dot{Q}_l$	(6)					
Ventilation power [W]	$P_V = p_V.V.n_d$	(7)					
Heat Demand							
Heat demand rate [W]	$\dot{Q}_h = \left(\dot{Q}_T + \dot{Q}_V\right) \left(\dot{Q}_S + \dot{Q}_o + \dot{Q}_e + \dot{Q}_l\right)$	(8)					
Specific heat demand rate [W/m ²]	$\dot{Q}_{s}'' = \dot{Q}_{h} / A_{N}$	(9)					

TABLE III

TABLE IV						
Exergy Calculati	MA	IN EQUATIONS OF EXERGY ANALYSIS				
	Quality factor room air [-]	$F_{q,air} = 1 - T_o / T_i$				
Envelope	Exergy load rate of the room [W]	$E_{x_{air}} = F_{q,air} \cdot \dot{Q}_h$	(11)			
	Heating temperature [°C]	$T_{heat} = 0.5(T_{in} - T_{ret})/\ln((T_{in} - T_i)/(T_{ret} - T_i)) + T_i$	(12)			
Indoor air	Quality factor air at heater [-]	$F_{q,heat} = 1 - T_{ref}[K]/T'_{heat}[K]$	(13)			
	Exergy load rate at the heater [W]	$\dot{E}x_{heat} = F_{q,heat}\dot{Q}_h$	(14)			
	Heat loss rate [W]	$\dot{Q}_{loss,HS} = \dot{Q}_{h} \cdot (1/\eta_{HS} - 1)$	(15)			
Heating system	Auxiliary energy rate [W]	$P_{aux,HS} = p_{aux,HS} \cdot \dot{Q}_h$	(16)			
	Exergy demand rate [W]	$\Delta \dot{E}x_{HS} = \left(\dot{Q}_h + \dot{Q}_{loss,HS}\right) / (T_{in} - T_{ret}) \left\{ (T_{in} - T_{ret}) - T_{ref} \ln(T_{in}/T_{ret}) \right\}$	(17)			
	Heat loss rate [W]	$\dot{Q}_{loss,dis} = (\dot{Q}_h + \dot{Q}_{loss,HS}) \cdot (1/\eta_{dis} - 1)$	(18)			
Distribution	Auxiliary energy rate [W]	$P_{aux,dis} = p_{aux,dis}.(\dot{Q}_h + \dot{Q}_{loss,HS})$				
	Exergy demand rate [W]	$\Delta \dot{E} x_{dis} = \dot{Q}_{loss,dis} / \Delta T_{dis} \left\{ T_{dis} - T_{ref} \cdot \ln(T_{dis} / (T_{dis} - \Delta T_{dis})) \right\}$	(20)			
	Required energy rate [W]	$\dot{Q}_{HP} = (\dot{Q}_h + \dot{Q}_{loss,HS} + \dot{Q}_{loss,dis}).(1 - F_S)/\eta_{HP}$	(21)			
	Auxiliary energy rate [W]	$P_{aux,HP} = p_{aux,HP} (\dot{Q}_h + \dot{Q}_{loss,HS} + \dot{Q}_{loss,dis})$	(22)			
Generation	Exergy load rate [W]	$\dot{E}x_{HP} = \dot{Q}_{HP}F_{q,S}$				
	DHW energy demand rate [W]	$P_W = V_W \cdot \rho \cdot C_p \cdot \Delta T_{DHW} \cdot no_o / \eta_{DHW}$				
	Exergy load rate of the plant [W]	$\dot{E}_{x plant} = (P_l + P_V) F_{q,el}$	(25)			
	Required primary energy input rate [W]	$\dot{E}_{p,tot} = \dot{Q}_{HP}.F_P + (P_l + P_V + P_{aux,HP} + P_{aux,dis} + P_{aux,HS}).F_{p,el} + P_W.F_{DHW}$	(26)			
Energy transformation	Additional renewable energy input rate[W]	$\dot{E}_R = \dot{Q}_{HP}.F_R + \dot{E}_{env}$				
	Total exergy input rate [W]	$\dot{E}_{xtot} = \dot{Q}_{HP}.F_{p}.F_{q,s} + (P_l + P_V + P_{aux,HP} + P_{aux,dis} + P_{aux,HS}).F_{p,el}$ $+ \dot{E}_{R}.F_{a,R} + P_W.F_{DHW}.F_{a,S}.DHW$	(28)			



Fig. 2 Energy flow from primary energy transformation to the environment

In Case 1, a condensing boiler is used for the heat generation with a maximum supply temperature of 70°C and its efficiency is taken as 0.95. For Case 2, an air heat pump is used with COP of 2.50 and a maximum supply temperature of 80 °C. The supply and return temperatures of the radiators are taken as 70°C and 60°C with a heat loss/efficiency of 0.95, respectively. Main assumptions and constant parameters of the analysis are given in Table V [13].

For the energy source in the primary energy transformation, the given parameters, F_p and $F_{q,s}$ are the figures of the primary energy factor and the quality factor of the energy source, respectively. FR is a fraction factor.

The total energy input rate per area in unit of W/m^2 is calculated by

 $\dot{E}''_{tot,pa} = \dot{E}_{tot} / A_N \tag{29}$

The total energy input rate per volume in unit of W/m^3 is calculated by

$$\dot{E}''_{tot,pv} = \dot{E}_{tot} / V_N \tag{30}$$

The total exergy input rate per area in unit of $W\!/\!m^2$ is calculated by

$$\dot{E}x''_{tot,pa} = \dot{E}x_{tot} / A_N \tag{31}$$

TABLE V Main Assumptions of the Energy and Exergy Analysis								
	Parameter	Unit	Symbol	V	alue			
	Air exchange rate	[ach/h]	n _d		0.4			
Heat Losson	Heat exchanger efficiency	[-]	η_V	(0.8			
neat Losses	Specific heat of indoor air	[kJ/kgK]	Ср	1.	.005			
	Density of indoor air	$[kg/m^3]$	ρ		1.2			
	Window frame fraction	[-]	F_{f}	(0.3			
	Total transmittance	[-]	gj	0	.58			
Heat Gains	Solar radiation: SE to SW, NW to NE Other directions	[W/m ²]	$I_{s,j}$		20 50			
	Emitted heat per occupant	[W/person]	\dot{Q}'_o		80			
	Specific internal gains of equipment	$[W/m^2]$	$\dot{Q}_{e}^{\prime\prime}$	2	2.05			
Other Have	Specific lighting power	$[W/m^2]$	p_l	2				
Other Uses	Specific ventilation power	$[W/m^2]$	p_V	0	.26			
	Temperature drop	[K]			<5			
Distribution	Heat loss/efficiency	[-]	η_{dis}	0	.86			
System	Auxiliary energy	[W/kWheat]	$p_{aux,dis}$	9	0.02			
Storage	Solar fraction	[-]	Fs		0			
	Radiator inlet temperature	[°C]	T _{in}		70			
	Radiator return temperature	[°C]	T _{ret}		60			
Heating System	Auxiliary energy	[W/kWheat]	$p_{aux,HS}$	(0.2			
	Max. heat emission	$[W/m^2]$	$p_{heat,max}$	1	100			
	Heat loss/efficiency	[-]	η_{HS}	0	.95			
				Case 1	Case 2			
	Efficiency	[-]	η_{CB}	0.95	2.5			
	Primary energy factor source	[-]	F _P	1.30	3			
	Quality factor of source	[-]	F _{q,S}	0.95 1				
Generation	Max. supply temperature	[°C]	T _{CB,max}	T _{CB,max} 70				
	Auxiliary energy	[W/kW _{heat}]	Paux,Gen	1.80	10			
	Auxiliary energy constant	[W]	Paux, gen, const	20				
	Primary energy electricity factor	[-]	$F_{P,el}$	3	3			

The total exergy input rate per volume in unit of W/m^3 is calculated by

$$\dot{E}x''_{tot,pv} = \dot{E}x_{tot}/V_N \tag{32}$$

The total energy efficiency of the system (%) is expressed as follows:

 $\eta_{sys} = \dot{E}_{building} / \dot{E}_{tot}$ (33)

The total exergy efficiency of the system (%) is expressed as follows:

$$\psi_{sys} = \dot{E}x_{building} / \dot{E}x_{tot} \tag{34}$$

The exergy destruction rate of the system (W), can be calculated from:

$$\dot{E}x_{dest} = (1 - \psi_{sys})\dot{E}x_{tot}$$
(35)

The exergy flexibility factor is calculated by

$$F_{flex} = \dot{E}x_{HS} / \dot{E}x_{tot} \tag{36}$$

The relation between the exergy efficiency (ψ) and the sustainability index (SI) can be given as follows:

$$\psi = 1 - 1/SI \tag{37}$$

This relation shows how sustainability is affected by changing the exergy efficiency of a process [13].

IV. RESULTS AND DISCUSSION

In this study, the performance of a family house with a volume of 326.7 m^3 and a net floor area of 121 m^2 , located in the city of Izmir, Turkey is evaluated in terms of energetic, exergetic and sustainability aspects. The indoor and exterior air temperatures are taken as 20°C and 1°C, respectively.

Using the data in Table V, and (1) and (2), the total heat loss rate is calculated to be 3770.72 W. The heat gain rates from solar, internal and other power demand (e.g. sum of lighting power and ventilation power) are obtained to be 335.44 W, 248.68 W and 275.98 W using (3)-(7), respectively. According to these data, the heat demand rate and the specific heat demand rate of the building calculated from (8) and (9) are 2744.66 W and 22.68 W/m², respectively.

An energy flow in the subsystems is calculated and given in Table VI and illustrated in Fig. 3.



Fig. 3 Energy flow diagrams for (a) condensing boiler, (b) air heat pump

The system requires a primary energy rate of 5559.7 W for Case 1 and 5019 W for Case 2, respectively in order to supply a total of 2744.66 W to the building. As can be seen in Table VI, the energy demand of the indoor air, the heating system and the distribution system are equal for all cases.

ENERGY AND EXERGY FLOWS IN THE SUBSYSTEMS OF THE STUDIED CASES							
Subsystems Studied Cases		Energy Fl	ow (W)	Exergy F	low (W)		
Subsystems (Studied Cases		Case 1	Case 2	Case 1	Case 2		
Input	1	5559.7	5019.0	5331.0	5019.0		
After primary transformation	2	3847.0	1673.0	3618.5	1613.0		
After generation	3	3369.1	3369.1	1032.3	1032.3		
After distributon	4	2889.7	2889.7	907.3	907.3		
After heating system	5	2744.7	2744.7	360.2	360.2		
After indoor air	6	2744.7	2744.7	177.9	177.9		
After envelope	7	2744.7	2744.7	0	0		

TABLE VI

The highest amounts of the heat loss rates occur in the primary energy transformation. In Case 2, after the primary energy transformation, an increase occurs. The explanation for this increase is that the amount of the renewable The total exergy demand rate is determined based on the methodology as followed in the energy demand calculation, but with exergy analysis. The exergy demand rates are calculated as 5331 W and 5019.0 W, respectively for Cases 1 and 2 (Table VI).

The exergy flow diagram of the system is shown in Fig. 4. As can be seen in Fig. 4, the amount of exergy is consumed in each component for all cases. While the flow of energy leaves the building envelope, as seen in Fig. 3, there is still a remarkable amount of energy left, but this is not true for exergy (Fig. 5). Therefore, the exergy flow at the last row of Table VI is required to be zero.



Fig. 4 Exergy flow diagrams for (a) condensing boiler, (b) air heat pump



Components

Fig. 5 Energy and exergy flow rates through components of Case 1

The variations of the energy and exergy loss rates through the components are illustrated in Fig. 6 and given in Table VII. The highest exergy loss rate (3406.0 W) occurs in the heat generation components of Case 2.



Fig. 6 Variation of energy and exergy loss rates through components

TABLE VII
ENERGY AND EXERGY LOSS RATES OF THE SUBSYSTEMS

ENERGY AND EXERCIT LOSS RATES OF THE SUBSTSTEMS							
Subsystems\ Studied Cases	Energy L (W	oss Rate	Exergy Loss Rate (W)				
-	Case 1	Case 2	Case 1	Case 2			
After primary transformation	1712.7	3346.0	1712.5	3406.0			
After generation	477.9	309.4	2586.2	2586.2			
After distributon	479.4	479.4	125.0	125.0			
After heating system	145.0	145.0	547.2	547.2			
After room	0.0	0.0	182.3	182.3			
After envelope	0.0	0.0	177.9	177.9			

Results of the energy and exergy analyses are summarized in Table VIII. The overall energy efficiencies of the studied cases are determined to be 49.4% and 54.7%. The overall exergy efficiencies, the flexibility factor and the sustainability index of Cases 1 and 2 are calculated to be 3.3%, 0.17 and 1.034, respectively.

V. CONCLUSIONS

In this study, comprehensive energy and exergy analyses for sustainable buildings are considered and applied to two different heating options (1) a condensing boiler, and (2) an air heat pump for a building in Izmir with a net area of 121 m². Their performances are compared through energy and exergy efficiencies. The energy and exergy results, the energy dispersals, the exergy flows and the exergy destructions are quantified and illustrated for comparison purposes.

The main conclusions drawn from the results of the present study may be listed as follows:

- The energy demand rate of the building is 2744.7 W. •
- The system requires primary energy rates of 5559.7 W and 5019 W for Cases 1 and 2, respectively.
- The exergy demand rates of the heating systems are determined as 5331 W for Case 1 and 5347.1 W for Case 2
- The highest exergy loss rate of 3406.0 W occurs in the heat generation components of Case 2.
- The overall energy efficiencies of the studied cases are calculated to be 49.4% and 54.7%.

The overall exergy efficiencies, the flexibility factor and the sustainability index of Cases 1 and 2 are calculated to be 3.3%, 3.5%, 0.17, 0.18 and 1.034, respectively.

Studied cas	es η _{sys}	ψ_{sys}	Ex_{dest}	Ė" _{tot,pa}	Ė" _{tot,pv}	$Ex''_{tot,pa}$	$Ex''_{tot,pv}$	F _{flex}	SI
	(%)	(%)	(W)	(W/m^2)	(W/m^3)	(W/m^2)	(W/m^3)	(-)	(-)
Case 1	0.494	0.0334	5153.12	45.95	17.02	44.06	16.32	0.1702	1.0345
Case 2	0.547	0.0354	4841.11	41.48	15.36	41.48	15.36	0.1808	1.0344
A cp Ė Ėx	N area (m ²) specific heat at c energy rate (W) exergy rate (W)	OMENCLATU	RE ure (kJ/kg.K)		f F g I I N	approximation f factor (-) total transmittan radiation intensi length (m) percentage of eq	actor (-) ce (-) ty (W/m ²) uipment resistance		

TABLE VIII RESULTS OF THE ENERGY AND EXERGY ANALYSES AND TOTAL ENERGY AND EXERGY INPUT PER AREA/VOLUME

nd	air exchange rate (1/h)	tot		total
no	number (-)	usf		useful
Р	power (W)	V		ventilation
р	specific power, pressure $(W/m^2, N/m^2)$	w		window, water
Ò	heat transfer rate (kW)	х		part x
Ř	pressure drop of the pipe (Pa/m)			
SI	sustainability index (-)	5	uper	scripts
Т	temperature (K)	over	r	dot rate
U	thermal transmittance (W/m^2K)	,	1664	viations
<i>i</i> v	volumetric flow rate (m^3/s)	71	-	
V	volume (m ³)	CO	P	coefficient of performance
~		DH	W	domestic hot water
Greek l	etters	ECI	BCS	energy conservation in buildings and community systems
17	energy efficiency (-)	prog	grami	me
		IEA		international energy agency
Ψ	exergy efficiency (-)	Low	vEx	low exergy
ρ	density (kg/m ³)			
Δ	difference			References
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pv	per volume			
q	quality			
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